

## STUDY OF THE INFLUENCE OF THE HYDRODYNAMIC REGIMES OF THE DIFFUSER-CONFUSER PROFILE PIPE ON THE HEAT EXCHANGE PROCESS

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### Abstract

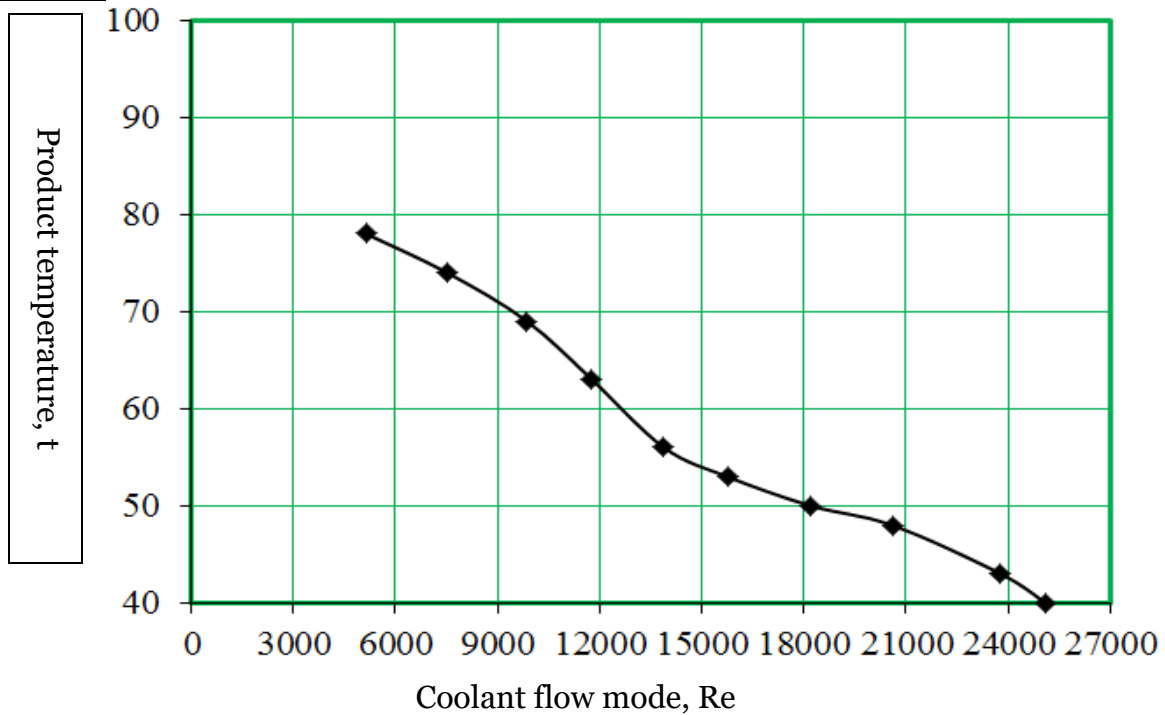
The article studies the impact of the shell-and-tube heat exchanger used in the oil refining industry, which is a hot topic today, on the hydrodynamic regimes of the diffuser-confuser profile pipe on the heat exchange process.

**Keywords:** Spherical concave tube, hydrodynamic regime, cooling agent, heat, confuser, diffuser.

### Introduction

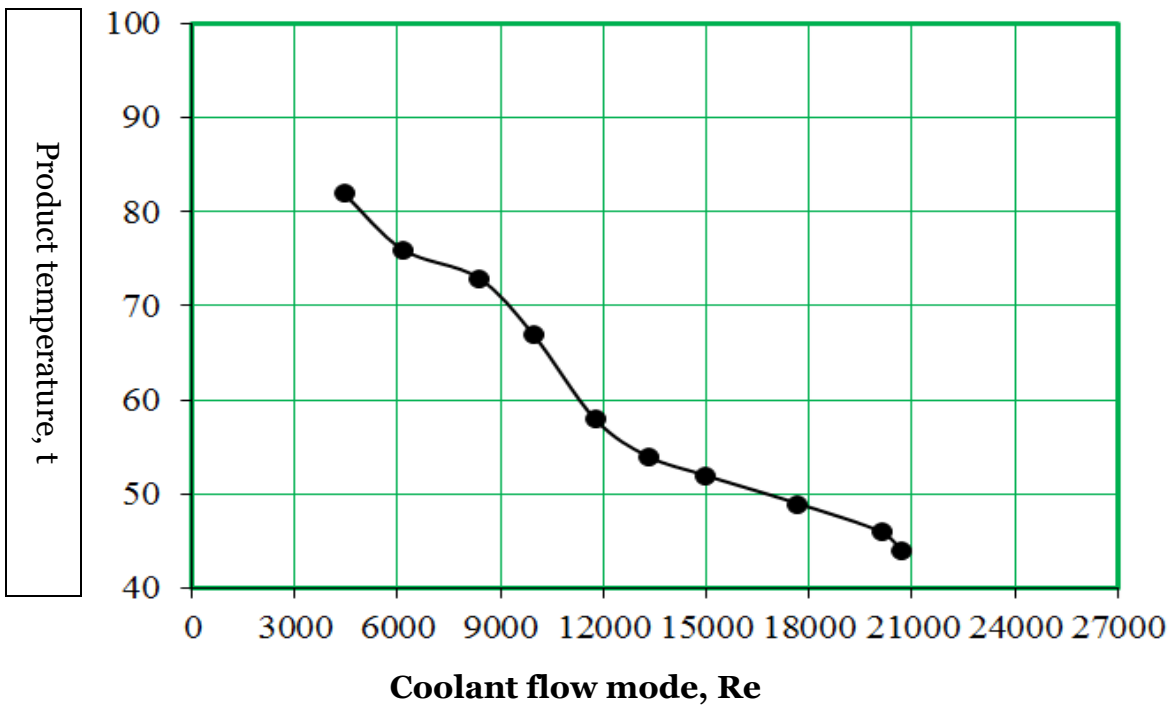
In researching the heat exchange process in shell-and-tube devices, the experiment's results and calculation on determining the hydrodynamic regimes of the spherical concave pipe and the existing calculation methods were used. In the conducted experiments, the following limits of variable factors, spherical concave length  $S=25$  mm, spherical concave radius  $R=10$ ; 20 and 30 degrees, the inner diameter of the pipe  $D=10$  mm and  $d=7$  mm, the temperature of the cooled product is  $100^{\circ}\text{C} \pm 2$ , the temperature of the heat exchange agent is  $20^{\circ}\text{C} \pm 2$ , and the density of the liquid is  $\rho_s=1000$  kg/m<sup>3</sup>.

Taking into account the influence of the external environment during the experiments, the temperature for the water and gas system was set at  $30^{\circ}\text{C} \pm 2$ . Based on the obtained experimental results, comparison graphs were constructed on the effect of heat exchange agent flow regimes on the heat exchange process. (Figures 1.1; 1.2 and 1.3)



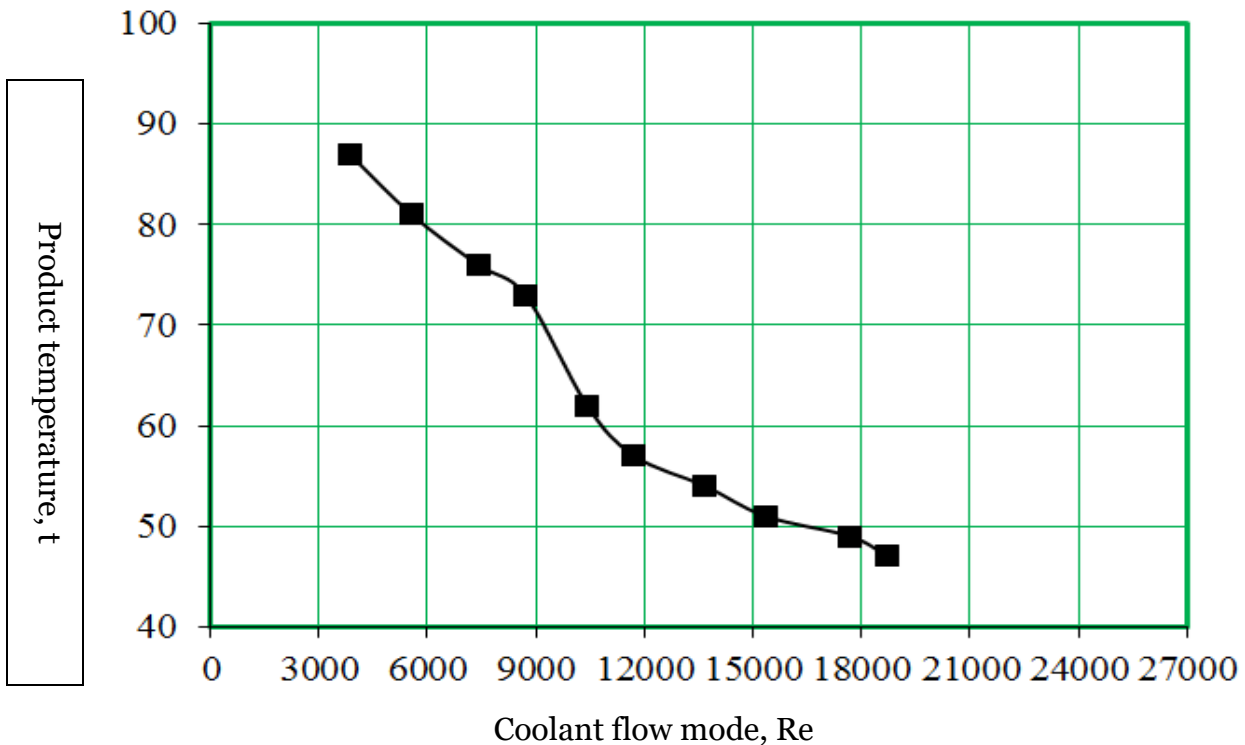
When  $a=15\text{gr-const.}$

**Figure 1.1. Dependence of the temperature of the cooled product on the flow mode of the cooling agent.**



When  $a=20\text{ gr-const.}$

**Figure 1.2. Dependence of the temperature of the cooled product on the flow mode of the cooling agent.**



When a=25 gr-const.

**Figure 1.3. Dependence of the temperature of the cooled product on the flow mode of the cooling agent.**

1.1; From the data given in Figures 1.2 and 1.3, it can be seen that when the spherical concave radius a=15 gr const and the speed of the heat exchange agent changes depending on the shape of the rotometer, the lower indicator of the flow regime at 5129 shows a decrease in the temperature of the product to 78 oS if, At 25087, the temperature of the product decreased to 40 °C at the high flow rate.

When the spherical concave radius a=20 gr const and the speed of the heat exchange agent changes depending on the shape of the rotometer, the product's temperature decreases to 82 °C at the lower indicator of the flow regime 4417. At 20660, the temperature decreases to 44 °C.

When the spherical concave radius a=25 gr const and the speed of the heat exchange agent changes depending on the shape of the rotometer, the lower indicator of the flow regime at 3855 shows a decrease in the product's temperature to 87 °C. At 18704, the temperature of the product decreased to 47 degrees Celsius.

The following empirical formulas were obtained for the results using the least squares method.

$$y = -08x^2 - 0,0033x + 94,99 \quad R^2 = 0,9887 \quad (1.1)$$

$$y = 08x^2 - 0,0046x + 101,76 \quad R^2 = 0,9816 \quad (1.2)$$

$$y = 07x^2 - 0,0056x + 108,59 \quad R^2 = 0,981 \quad (1.3)$$

The following values were adopted as optimal parameters in the experimental studies conducted to use different parameters of the concave radius of the spherical concave pipe and evaluate its effect on the efficiency of the heat exchange process. The mathematical planning method and the PLANEX programs were used to obtain the values [57-59].

### According to him:

The temperature of the product decreases to 59 C when the radius of the spherical concave is 22 gr, the consumption of the cooling agent is  $Q=0.188$  m<sup>3</sup>/hour, and the speed of the cooling agent is  $\omega=1.28$  m/s. This situation fully satisfies the students of technological regulation. In addition, it is ensured that the efficiency of using a cooling agent increases by 1.75 times.

### Conclusions

- Cooling agent consumption, speed and flow regimes in the pipe were experimentally determined in different parameters of the radius of the pipe with a confusor-diffuser profile;
- The effect of flow regimes on product temperature was studied;
- Optimal parameters of the pipe profile were based on the experiments using the mathematical planning method;
- It is ensured that the efficiency of using the cooling agent increases by 1.75 times.

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